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by Adi Winarta

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A Preliminary Investigation of Oscillating Heat Pipe Using Aluminum Capillary Tube

Adi Winarta^{1, a)} and Nandy Putra^{2, b)}

¹Department of Mechanical Engineering, Politeknik Negeri Bali, 80364, Bali, Indonesia

²Department of Mechanical Engineering, Universitas Indonesia, 16425, Depok, Indonesia

^{a)} Corresponding author: adi.winarta@pnb.ac.id

^{b)} nandy.putra@ui.ac.id

Abstract. Oscillating Heat Pipe (OHP) is one of the newest heat pipe family which have a potential application at space and aerial application. This application usually has strict constrain in weight and flexibility. In this early-stage studies, an aluminum OHP was tested with different filling ratio of distilled water (DI) water as working fluid. Method of vacuum charging was applied to injected the working fluid into the heat pipe properly. Aluminum OHP was constructed with 12 turns and formed into close loop. The heat supplied to the evaporator was varied from 10 until 60 watts. The result show that there is an effect of generation non-condensable gas which obstruct the heat transfer performance of aluminum OHP.

INTRODUCTION

In recent years Oscillating Heat Pipe (OHP) as one of the two-phase heat transfer technologies has attracted the attention of many scientists. With the excellent performance capabilities, simple structure and low production costs, OHP promises huge potential in a wide range of heat transfer applications [1, 2]. This technology was first introduced by Akachi et al. [3] on USA Patent in 1990. Although the fundamental concept of OHP has been claimed by Smyrnov and Savchenkov at Russia Patent on 1975 [4]. In 2003, Smirnov returned to patent the method, construction and basic concept of this heat pipe type [5] in USA Patent. In OHP, the heat transfer from evaporator to condenser was generated by oscillations or circulation of the working fluid inside the OHP. This oscillations or circulation of the working fluid was caused by pressure difference at the evaporator and condenser. This occurs due to heat input at the evaporator section and rejected heat at the condenser. The evaporator heat input would create the bubble growth and simultaneously, rejected heat at the condenser would result bubble collapse. This condition, which is coupled by the distribution of the working fluid in the form of the composition of liquid and vapor, would cause complex displacement in the form of pulsating and oscillating movements in the OHP [6].

The OHP research in the last decade focused on some aspects, such as flow pattern of working fluid, thermal performance, global orientation, gravity effects and mathematics analysis [6-13]. From the flow pattern study, we also known if some patterns such as bubbly flow, slug flow, annular and semi annular occur during the operational process [10, 12]. Each pattern has different heat transfer characteristics which would affect the performance of OHP [14]. As one of the prime parameters, heat input to the evaporator greatly affects the flow pattern and contribute to the oscillating motion of liquid and vapor plug inside the OHP tube. Certain flow pattern causes a different heat transfer potentiality. When heat input was rising, heat transfer capability would also rise as a result of stronger oscillating movement [15]. Observation of the flow pattern such as oscillation, circulation, changes in flow direction and unidirectional flow of this circulation was closely associated with the change of heat input [16].

Observations visualization on OHP typically uses material with transparent tube. However, the use of these materials has some drawbacks such as transient temperature that would be difficult to recognize due to its low thermal conductivity [17]. Karthikeyan et al. [18] made observations with thermograph technique for the thermal profile of working fluid of the OHP to obtain thermal performance relationship with the character of the flow pattern. Their work used water as working fluid with filling ratio 60% and the OHP has 10 turns. Their results showed that the

Infrared thermograph was a very interesting tool for transient heat transfer conditions such as OHP. In this work, an oscillating heat pipe which made from aluminum capillary tube was tested using different filling ratio (45%) of OHP with water as working fluid. The performance and effect of aluminum as heat pipe container was observed and analyzed in this first stage work.

METHOD

Experimental Setup

The structure of the OHP was made by capillary tube with inside and outside diameter 1.6 and 2.18 mm respectively. The capillary dimension of pipe tube is used to ensure the formation of the liquid and vapor slug regarding with maximum diameter formula as shown in equation 1 [3] below:

$$d_{max} = 1.8 \cdot (\sigma / (\rho_l - \rho_v))^{1/2} \quad (1)$$

Figure 1 shows the schematic of the experimental setup of OHP test. The dimension of OHP was 230 mm x 110 mm with 10 turns. Evaporator, adiabatic and condenser length were 40, 120 and 70 mm respectively. The walls of each part of this section (evaporator, adiabatic and condenser) were solder with thermocouple type K 0.3 mm in diameter, with the $\pm 0.5^\circ\text{C}$ accuracy. To provide the heat input to the evaporator section, a pair of copper block with semicircular groove were made fix into evaporator section. The copper block has dimension of 131.5 x 5 x 40 mm³ and semicircular groove is manufactured in order to improve thermal contact with round geometry of pipe. Thermal paste was applied between the capillary tube and copper block to reduce thermal contact resistance. Cartridge heater (Omega CSH-104 400) was used as a heat source for the evaporator section. The heater was inserted into aluminum block through interference fit hole. Between these two metal blocks (copper and aluminum) stainless steel block with dimensions 131.5 x 25 x 40 mm³ was inserted as conduction block. Each side of the stainless-steel blocks which contact with copper and aluminum were soldered with the thermocouple to measure the temperature difference. The conduction stainless steel block helps calculate the input heat (Q) for the evaporator section based on the equation 2.

$$Q = k \cdot A \cdot \Delta T / L \quad (2)$$

With k the thermal conductivity of stainless steel, ΔT is temperature difference between each side of stainless steel which is in contact with copper and aluminum block and L is thickness of the stainless steel. All the experimental data captured at bottom heating mode or it means the evaporator section placed at the bottom of test section.

A thermostatic bath was used to supply the cold water with $\pm 15^\circ\text{C}$ for cooling the condenser section in the acrylic cooling box. The mass flow rate of cold water was measured using a rota meter (± 450 mL/sec). Some type-K thermocouples (bead diameter 0.3mm and accuracy of $\pm 0.1^\circ\text{C}$) were used to measure wall temperature, i.e., two points (T1 and T2) at evaporator, two points (T3 and T4) at adiabatic and two points (T5 and T6) at part of condenser. To record temperature data, we used NI-9174, NI-9219 and LabVIEW data acquisition with sampling rate of 3 data per second. This refers to the characteristic frequency range of internal OHP oscillating phenomena tube 0.1 and 3 Hz [19]. Temperature observation was also accomplished by using an infrared camera (FLIR i50 with 140 x 140 pixels image resolution). The thermography observation would be done to the painted black part of adiabatic, to give a higher emissivity ($\epsilon=1$).

Charging fluid in OHP was done using back filling method [20]. OHP is vacuumed first, then DI Water as working fluid was injected into it. Filling ratio was the ratio between injected fluid volume with OHP tube total volume. The ratio of the working fluid used was 45%.

Total thermal resistance of OHP (R_{tot}) is the ratio of the temperature difference between the evaporator and condenser ($T_{evap} - T_{condenser}$) then divided by the heat input. The equation for calculating (R_{tot}) is given as follows:

$$R_{tot} = \frac{\bar{T}_{evap} - \bar{T}_{condenser}}{Q} \quad (3)$$

Where,

$$\bar{T}_e = \frac{T_1 + T_2}{2}, \quad \bar{T}_c = \frac{T_3 + T_4}{2} \quad (4)$$

Effective thermal conductivity (K_{eff}) computed by

$$K_{eff} = \frac{L_{tot}}{A_{cr}} \frac{1}{R_{tot}} = \frac{L}{A_{cr}} \frac{Q}{(\bar{T}_{evap} - T_{\infty})} \quad (5)$$

$$\text{Where, } A_{cr} = n \cdot \pi \cdot \frac{d_{out}^2}{4} \text{ and } L_{tot} = \frac{1}{2}(L_e + L_c) + L_a \quad (6)$$

A_{cr} , \bar{T}_{evap} , T_{∞} , L_e , L_c , L_a respectively are area of tube cross section, average evaporator temperature, fluid cooling temperature evaporator length, condenser length, adiabatic length.

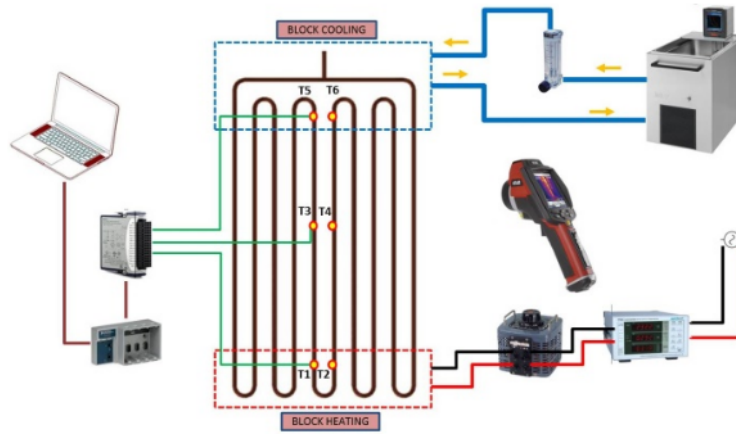


FIGURE 1. Experiment set-up

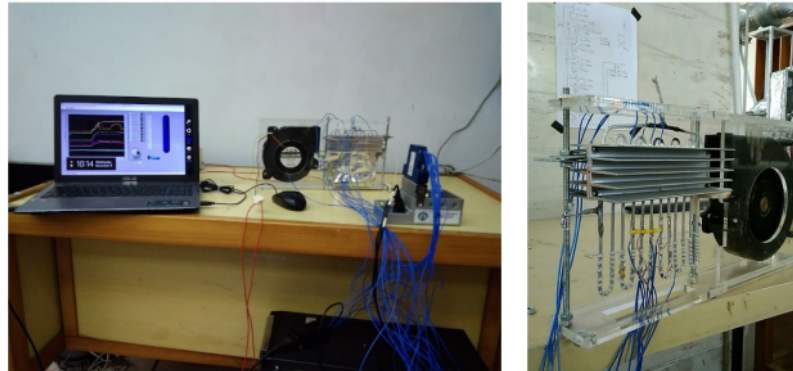


FIGURE 2. Implementation of experiments in the laboratory

RESULT AND DISCUSSION

The profile temperature distribution observed by Karthikeyan et al [18] with infra-red technique clearly indicates that there were different flow patterns on OHP. By using infra-red camera and thermocouple temperature observation this test seeks to observe transient temperature distribution of the OHP at various heats input. Without the use of visualization techniques, it was difficult to determine the dynamic behavior of liquid slug and slug of vapor inside the tube of OHP [21] at the appropriate heat input (Figure 3).

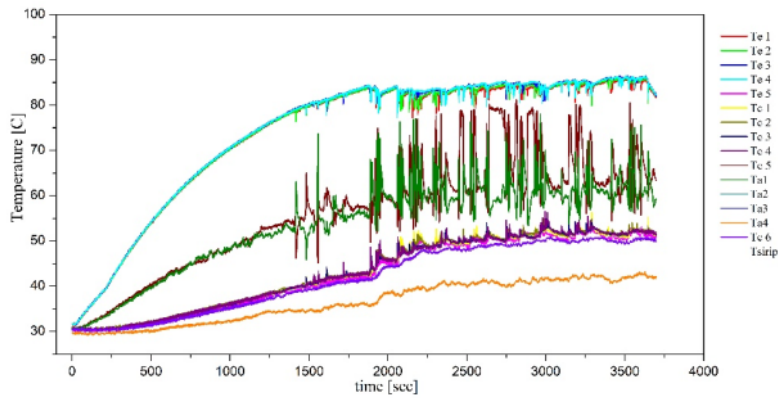


FIGURE 3. Test no 1 to aluminium OHP with DI water as working fluid and heat load 25 watt

Figure 3 shows the global temporal evolution of the evaporator and condenser temperatures for all heat input variation. Each of heat input as shown in Figure 2 would be analyzed separately (see Figure 4).

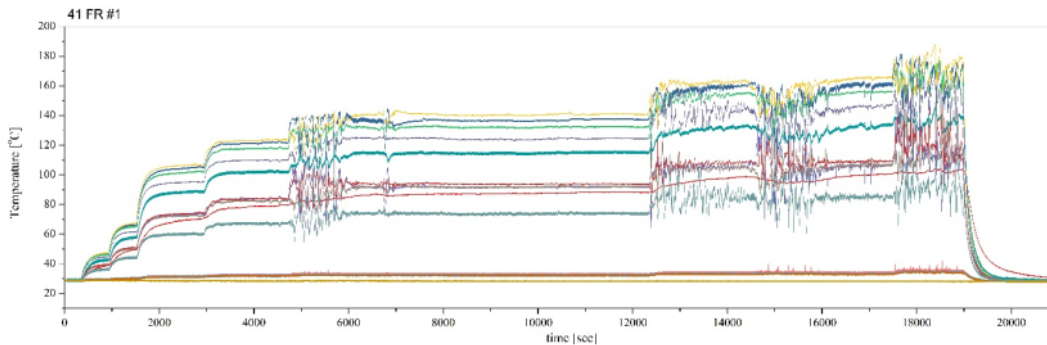


FIGURE 4. Test no 1 to aluminium OHP with DI water as working fluid and heat load 25 watt

Start-up process of oscillating heat pipe as observed by Xu et al [22] very easily to do when using this technique (pairing thermocouple and infra-red). It can be clearly concluded that there had no motion of the working fluid at all section in the OHP. The gradual increase temperature of the evaporator and condenser due to conduction heat transfer process at copper capillary tube. There's not enough heat energy to produce bubble growth at the evaporator section to initiated pumping motion from the pressure difference.

Small temperature fluctuations on the evaporator and condenser were started at the 24 Watt heat input. Conversely from the infra-red picture the fluid oscillation motion clearly seen from different temperature spatial distribution on each adjacent channel. These thermal footprints indicate the occurrence of macro working fluid movement on adiabatic section. Although the oscillation still in random motion due to the device it is not fully initiated or intermittent oscillations. In evaporator, the temperature fluctuation occurs with lower amplitude than in condenser. These temperature fluctuations in the evaporator and condenser indicated the movement of liquid slugs and vapor plug. Heat absorption which generates bubble growth was taking place at a relatively constant temperature. Consequently, evaporator temperature did not change much and tend to look steady. While in the condenser, temperature fluctuations amplitude appears higher due to the difference between the high temperature vapor slug flow and very low condenser cooling temperature (15°C). Sensible heat dominated the heat rejection at the condenser cooling section. The more vigorous temperature fluctuations occur in the next heat input rise. Therefore, decreasing

thermal resistance occurred at 36 Watt to 47 Watt heat input due to the higher frequency of oscillation of the working fluid (Figure 5).

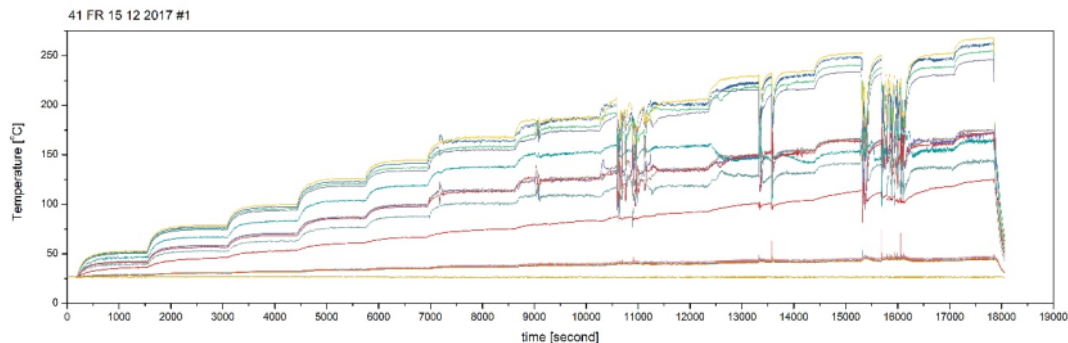


FIGURE 5. Test no 1 to aluminium OHP with DI water as working fluid and heat load 25 watt

Figure 5 shows the evolution of the temperature on 51 watt of heat input. From the graph, we can see if the evaporator's temperature tends would be steady at an average of 101.15 °C, which was indicates the absorption of heat by the heat pipe. The presence of temperature fluctuations at the evaporator and condenser also supports this case. The high amplitudes fluctuation on the condenser (20-22°C) is shown an exchange of heat due to the oscillating movement of the liquid slug. Temperature fluctuations that occur in the evaporator were much lower than the temperature fluctuations in the condenser section. This may indicate a bubble growth at the evaporator section which creates sufficient pumping action to move the liquid slug in oscillatory motion. Oscillation motion of liquid slug and vapor slug can be seen from the thermal footprint in Figure 5.

The frequency of temperature fluctuations on the condenser and evaporator higher at 65 watts of heat input. The increase in heat input provides sufficient energy to the liquid slug momentum so that changes in flow patterns of oscillation into circulation. This flow pattern changes lowers thermal resistance resulting from OHP. The circulation flows of working fluid increasing heat transfer performance of the OHP. There are sufficient decreases thermal resistance from increasing heat load from 51 to 65 Watt.

From temperature fluctuations and thermogram, it can be said that during circulation the liquid slug also oscillates axially. It was also stated by Borkar et al. [16] that the proper definition for this movement was "oscillatory circulation" or often said as bulk circulation. Oscillatory movement of the working fluid circulation can change direction and may also have a fixed direction. Raising the heat load to 88 Watt will augment the frequency of temperature fluctuations in the evaporator and condenser. The average temperature of the evaporator increases around 102.2°C. Rising frequency fluctuations resulted in a decrease in thermal resistance. At 109 watts of heat load, evaporator and condenser has a temperature fluctuation frequency remains high. However, the average temperature evaporator will rise to 106.6°C. The average temperature of the condenser also increased from 34.2°C the heat input 88 Watt became 41.47°C the heat input 109 Watt. The raise of average temperature can be seen on the temperature distribution in the infra-red camera picture. From the thermal point of view, the entire surface of the OHP has higher temperature. This resulted in the accession of the working fluid vapor fraction.

CONCLUSION

We have made a copper OHP using water as working fluid with filling ratio of 45% and 10 turn at evaporator and condenser. From the experimental work, we summary some major conclusions as follows:

1. Spatial thermal distribution temperature able to provide qualitative identification picture for analyzing the flow patterns appear inside OHP tube. The occurred flow pattern was depending on the heat input supplied. The qualitative and quantitative analysis of this flow pattern were made by combining thermocouple temperature data observation and Infra-red thermography. There are three types of flow pattern could be clearly identified with these methods i.e. oscillating motion of capillary slug, circulatory oscillation or bulk circulation of slug flow and circulation of annular flow.

2. The thermal resistance of the OHP tends to decrease with increasing of input level. The effective thermal conductivity of OHP at 142 Watt was 8 times higher than pure copper metal.
3. The experiment is conducted with the working fluid of water, filling ratio of 40% and a high stage heat input, and the dry out conditions was reached at 142 Watt heat input. The dry out process can be seen from the spatial distribution of OHP transient surface temperature and qualitatively can be captured easier by infra-red cameras.

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